

Physical limitations induced by a wheat bran-based medium for the production of biopesticides by *Bacillus thuringiensis serovar kurstaki*

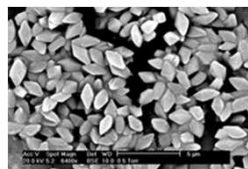
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Biopesticide production: Why and how?



Btk Lip and BLB1



Citrus plants

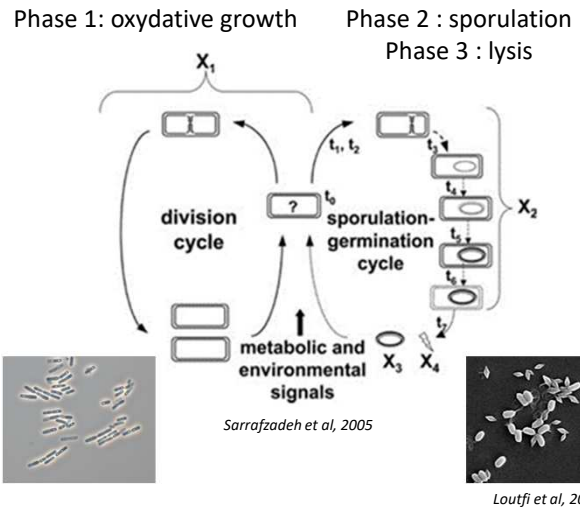
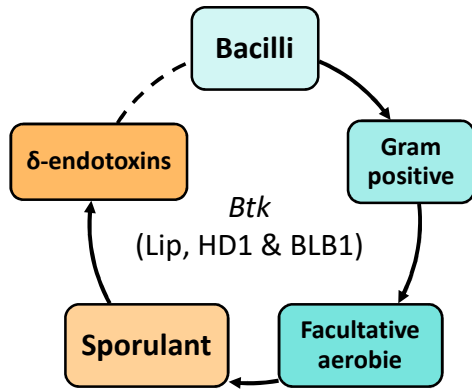


Pests

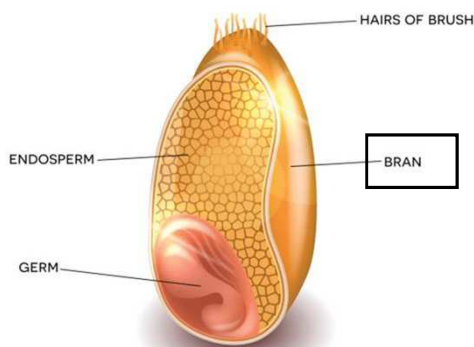
Phyllocnistis citrella & Prays citri

PHYTOXOGEN
~~X~~

Bacillus thuringiensis var kurstaki (Btk)



Wheat bran (WB): a good medium?



LOW COST



HUMAN NUTRITION

(Balandran et al, 2015)



HIGH YIELD

(Rahbani et al, 2014)



Meets *Btk* full nutritional requirements (Onipe et al, 2015)

Scientific background & objectives

Production of Btk δ -endotoxins in a wheat bran based medium

Comparison of the bioperformances in different media (SSM & WB)

(Mounsef et al. 2014)

Impact of WB granulometry

WB sieving → flask culture → optimal growth conditions
→ [WB]=73.6 gmh/L, pH=7, 248 rpm, Tp=30°C

(Abboud et al. 2017)

Identification of nutritional limitations

Biochemical analysis of the WB : starch, proteins, elemental composition
Determination of the fermentable fraction & the limiting nutrient

(MSc Al Kassis 2020,
MSc Barssoum 2021
MSc Nasseridine 2021)

Investigation of the process physical limitations

Granulometry, rheometry, settling kinetics and scale-up

(Barssoum et al, 2022)



Studying of the **physical limitations** generated by the media :

(i) During the **crucial steps** of the **process** (oxydative growth, sporulation and lysis)

(ii) **Simulation** of the process using a **dynamic model**

→ Parameters : morphology, rheometry and solid-liquid separation

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The technological itinerary of the substrate (WB)

Sieving

- Class 1 (>850 μm): <1%
- Class 2 (500-850 μm): 19.9%
- Class 3 (250-500 μm): 60.5%
- Class 4 (<250 μm): 19%

Culture

- WB suspension
- Heat treatment (HT)
- Inoculation (Flask)
- Solid-liquid separation (insoluble fraction, permeate)

Analyses

- Chemical: elemental composition (\pm culture), proteins, **starch** (- culture)
- **Physical: Morpho-granulometry** (- HT, + culture), **solid-liquid separation** (\pm HT, + culture), **rheometry** (+ HT, - culture)

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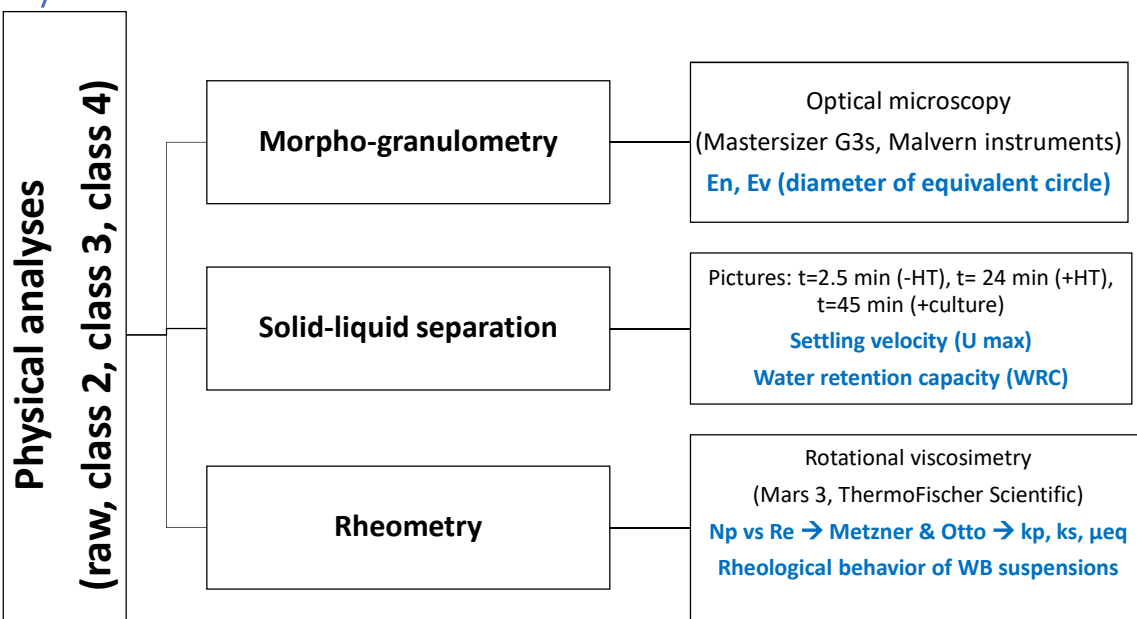
Chemical characterization of the WB

Class	Diameter (μm)	starch (g/g DM)	Proteins (Nitrogen Kjeldahl) (g proteins /g DM)	Elemental composition (%w/w)				
				C	H	O	N	Ashes
2	500-850	0.173 (± 0.35)	0.145 (± 0.012)	44.21 (± 0.19)	6.50 (± 0.12)	35.62 (± 0.45)	2.60 (± 0.23)	3.70 (± 0.12)
3	250-500	0.144 (± 1.35)	0.127 (± 0.014)	45.34 (± 0.08)	6.46 (± 0.04)	37.89 (± 0.44)	2.48 (± 0.04)	4.28 (± 0.12)
4	<250	0.347 (± 0.47)	0.155 (± 0.016)	42.40 (± 0.04)	6.61 (± 0.12)	34.60 (± 0.37)	2.61 (± 0.24)	3.23 (± 0.12)

- **Proteins & elemental composition: independants** from the **particle size**
- **Starch concentration** \searrow when the **particle size** \nearrow

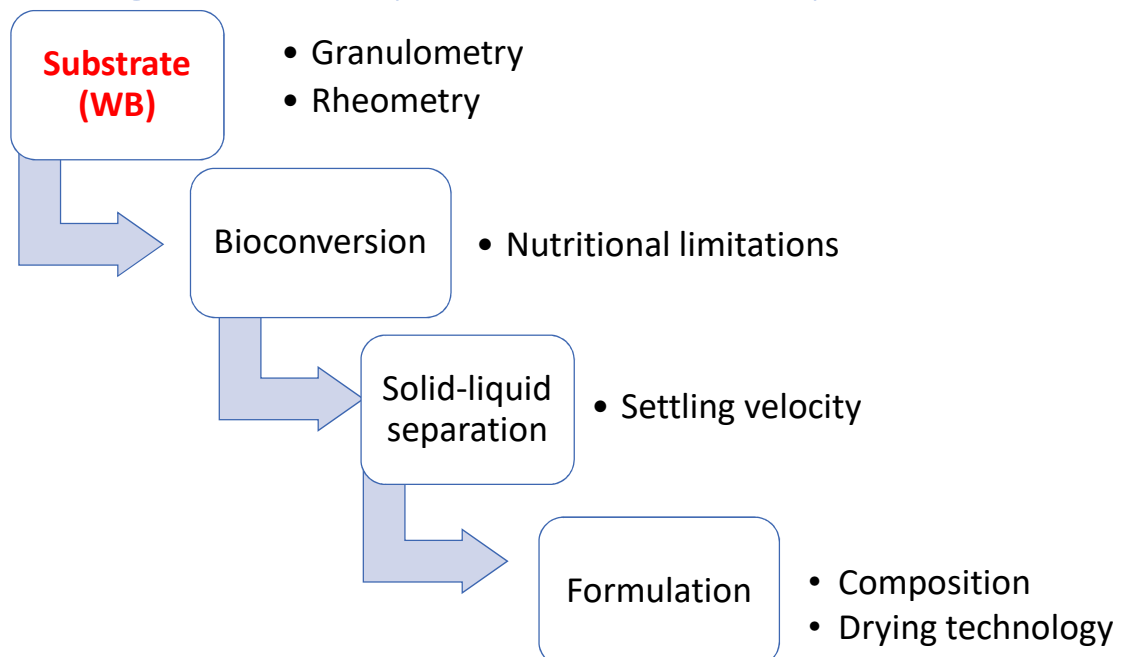
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Physical characterization of the WB



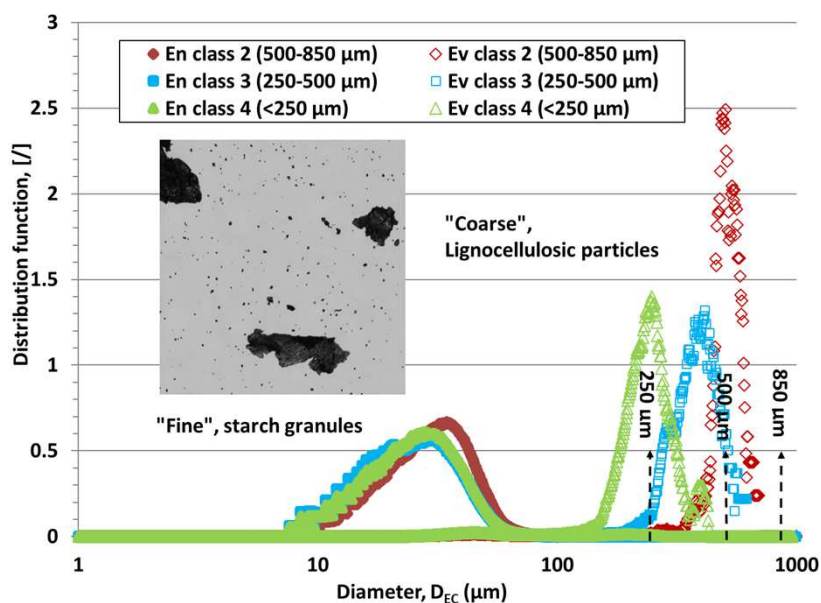
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Technological itinerary and down stream process (DSP)



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Morpho-granulometry of the WB particles

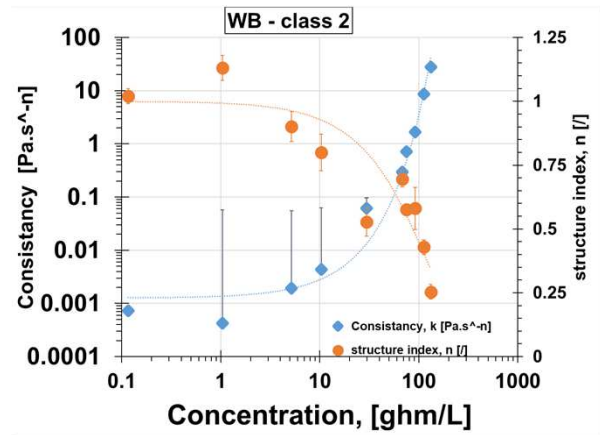
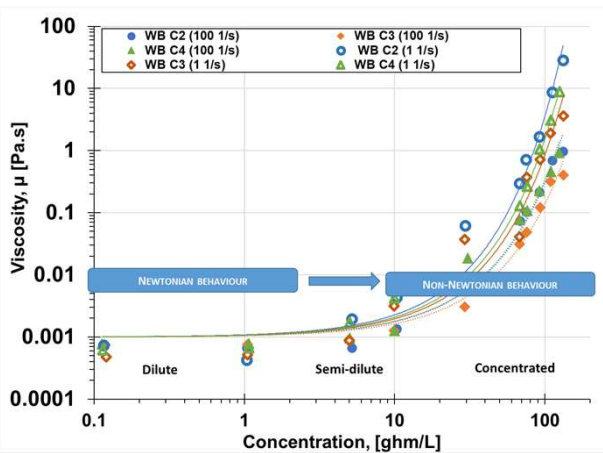


- Two populations: fines (**ovoidal** shape) and coarse (**angular** shape)
- **Distribution :**
 - En(dec) → **Fine population**
 - Ev(dec) → **Coarse population****(effect of sieving)**

- **Fines** → starch granules
- **Coarse** → lignocellulosic particles
- **Heat treatment** → starch granules liberated

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Rheological behavior of WB suspensions

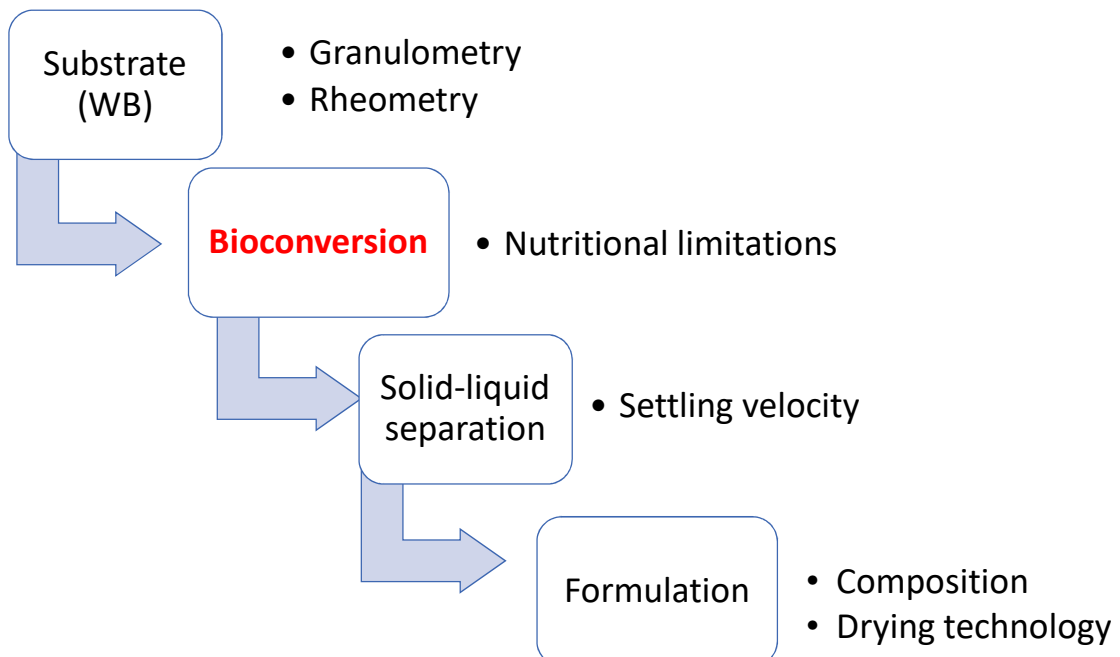


- Dilute regime: **Newtonian** behavior
- Concentrated regime : **shear- thinning** behavior
- $\mu_{Cl2} > \mu_{Cl3} > \mu_{Cl4}$
- **Balance** between **starch** and **granulometry** effects

- Concentration ↗ → K ↗
- Concentration ↘ → n ↗
- Incertitude (methodology)

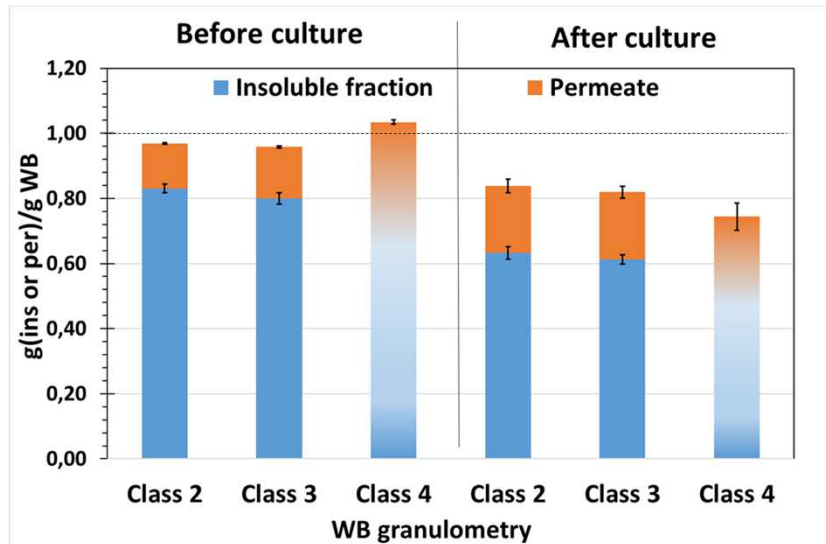
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Technological itinerary and down stream process (DSP)



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What is the fermentable fraction?



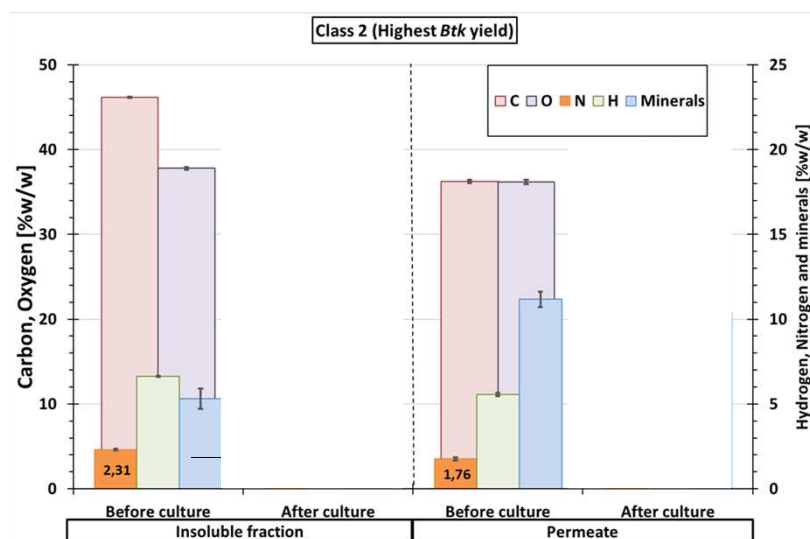
- Insoluble fraction: concentration ↓
- Permeate: concentration ↗
- Fermentable fraction ??

	Fermentable fraction (g/ gdm WB)	Starch (g/ gdm WB)
Cl 2	0.32	0.17
Cl 3	0.36	0.14
Cl 4	0.51	0.34

- Lignocellulosic fraction: partial consumption

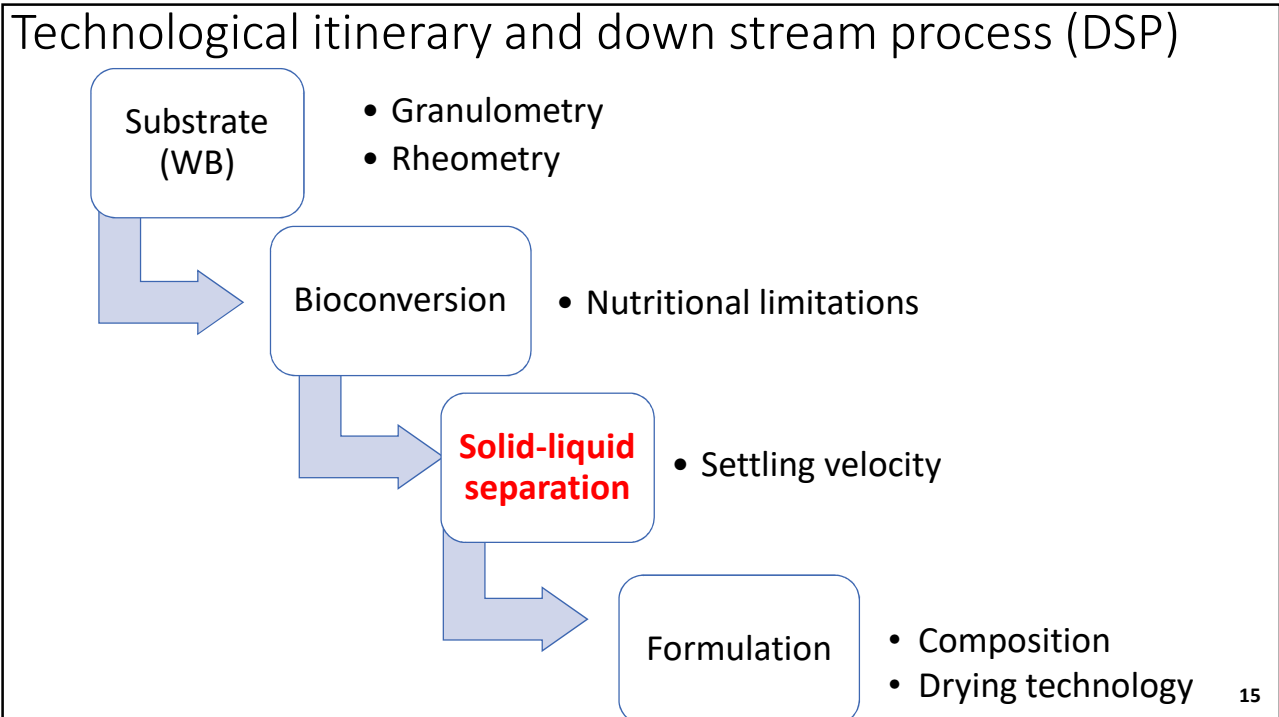
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Is there a nutritional limitation during the culture?

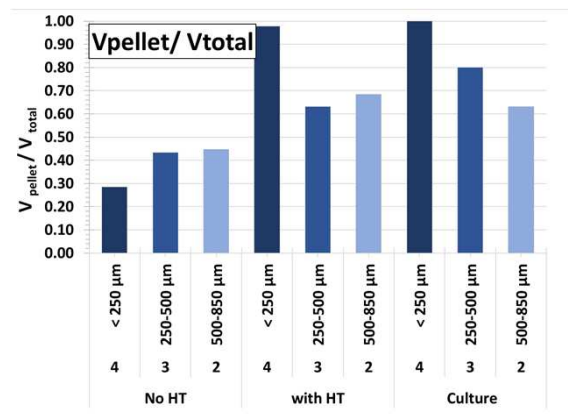
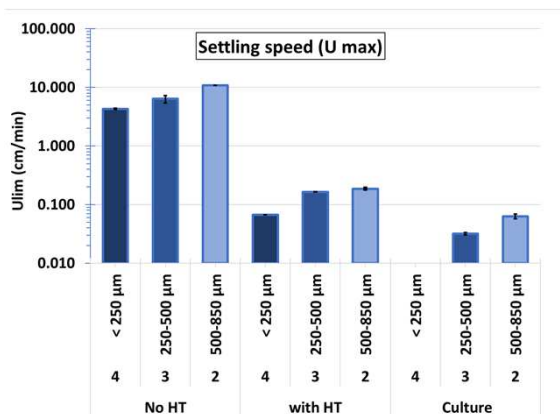


- Insoluble fraction: N ↘ → substrate proteins consumption
→ N in substrate > 40% N accessible
- Permeate: N ↗ → biomass production
- N: limiting nutrient

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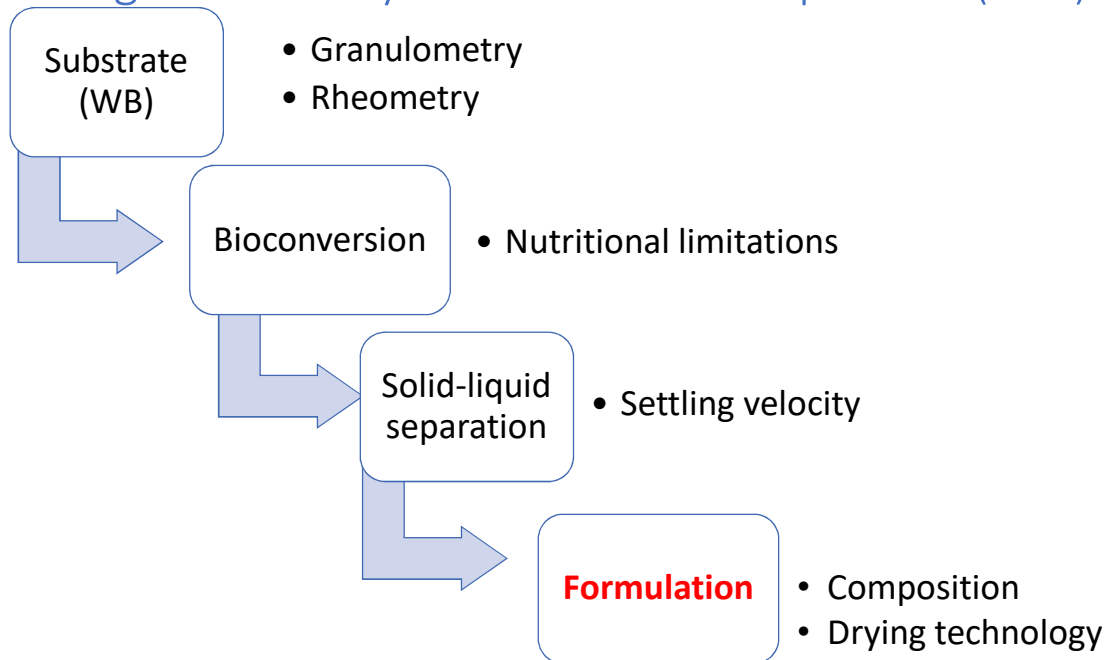
Focus on DSP: solid-liquid separation



- Particle size ↗ → U_{lim} ↗
- Heat treatment → starch colloids → U_{lim} ↘
- Culture → Starch consumption by *Btk*

- Heat treatment: V_p/V_t class 4 > class 3 > class 2
- Culture → V_p/V_t increases

Technological itinerary and down stream process (DSP)



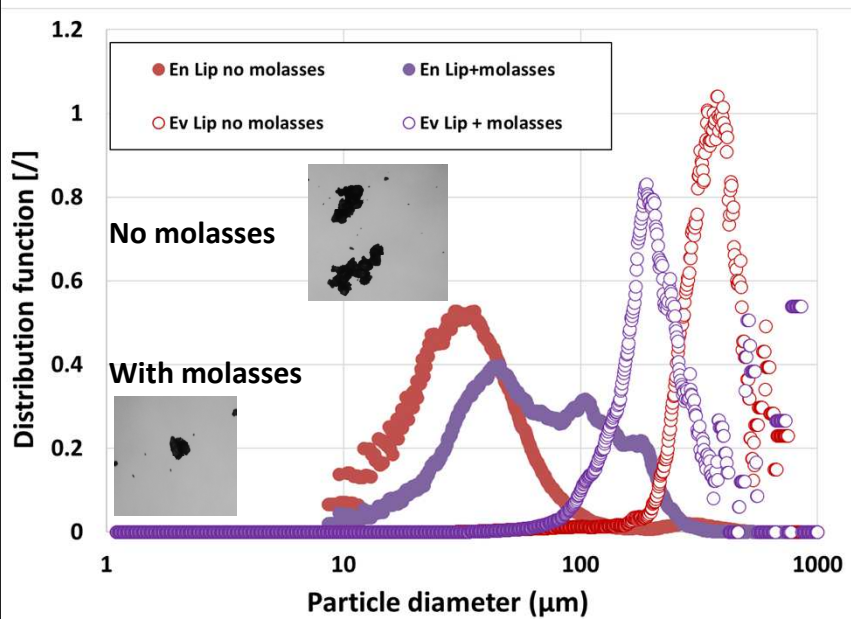
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Focus on DSP: formulations & drying technology

Strain	Number of dry formulations	Composition of the dry formulation	Drying technology
<i>Btk Lip</i>	Two	<ul style="list-style-type: none"> • with molasses (one formulation) • without molasses (one formulation) 	Fluid bed drying
<i>Btk BLB1</i>	Two	<ul style="list-style-type: none"> • with molasses (one formulation) • without molasses (one formulation) 	Freeze drying +mechanical grinding

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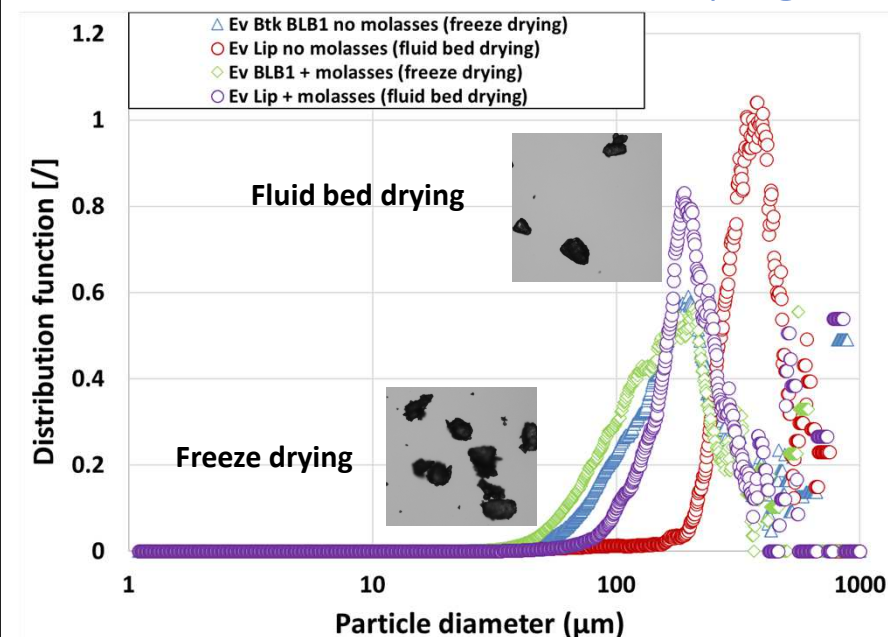
Focus on DSP: effect of molasses on formulations



- Two populations: fines & coarse
- En: fines (10-100 μm)
- Ev: coarse (100-1000 μm): aggregates of lactose
- En: molasses \rightarrow bigger aggregates
- Ev: molasses \rightarrow smaller aggregates
- Addition of molasses \rightarrow dispersion of coarse particles

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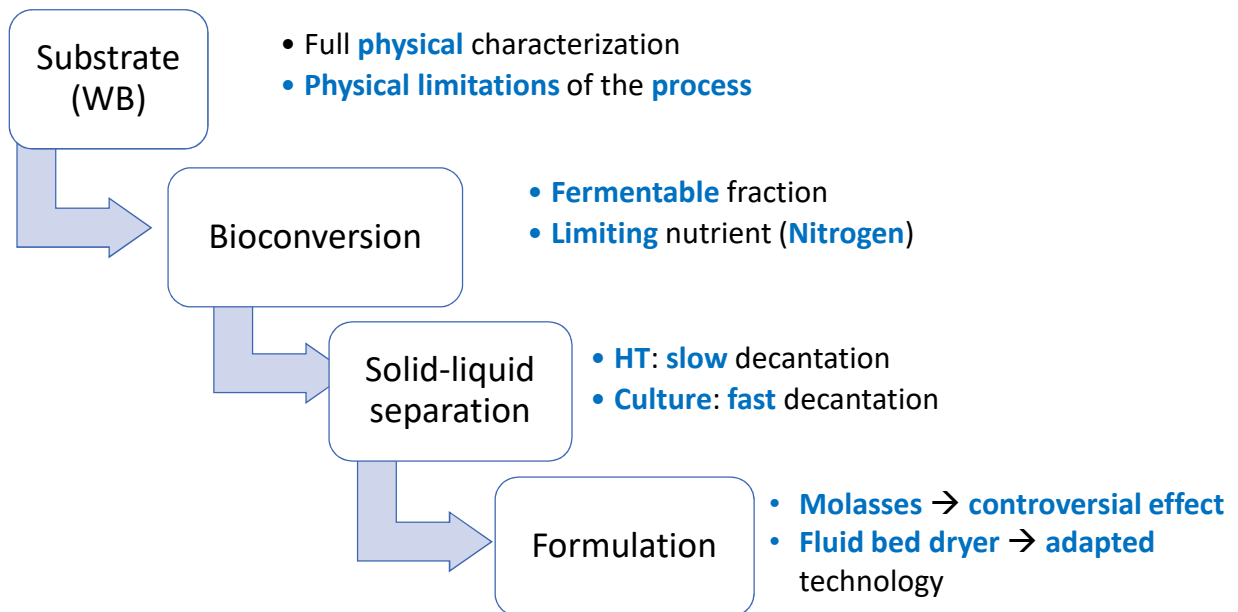
Focus on DSP: effect of the drying technology



- Fluid bed drying \rightarrow no mechanical attrition \rightarrow bigger aggregates
- Freeze drying \rightarrow mechanical attrition \rightarrow smaller aggregates
- Freeze drying: breaks the particles heterogeneously
- Fluid bed dryer is more adapted for the process

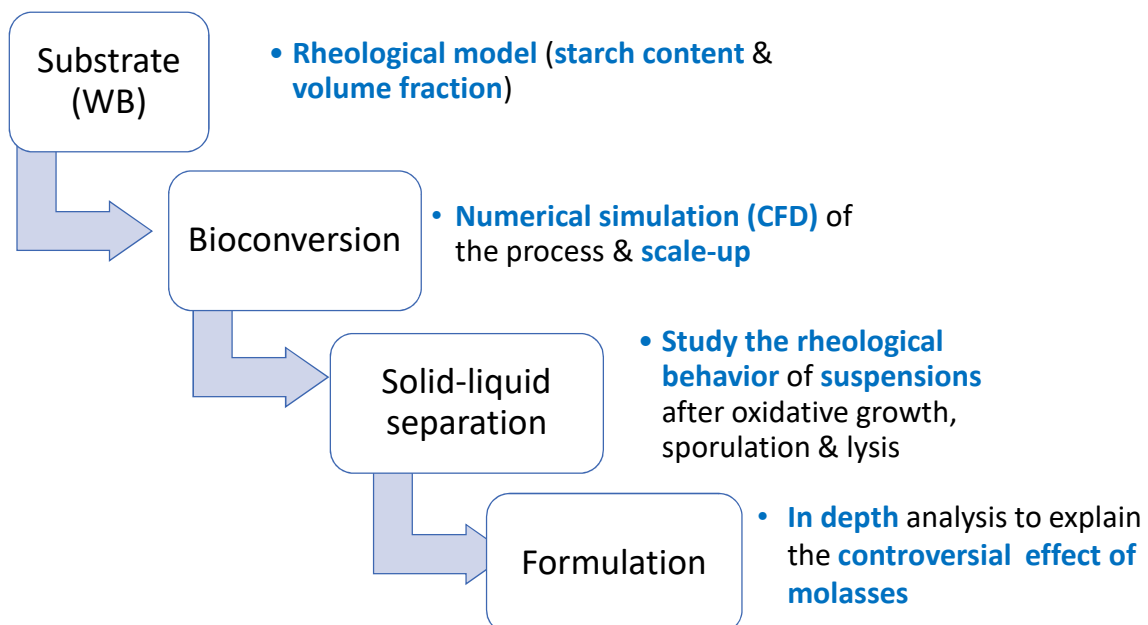
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Conclusions



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Perspectives



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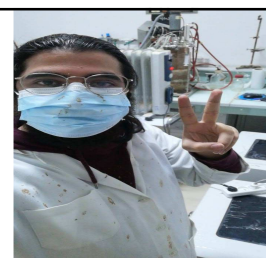
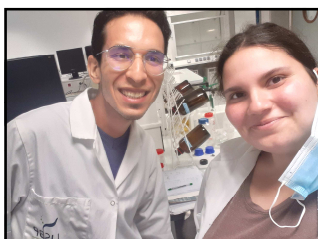


The organizers of JIB 2022



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Thank you for your attention

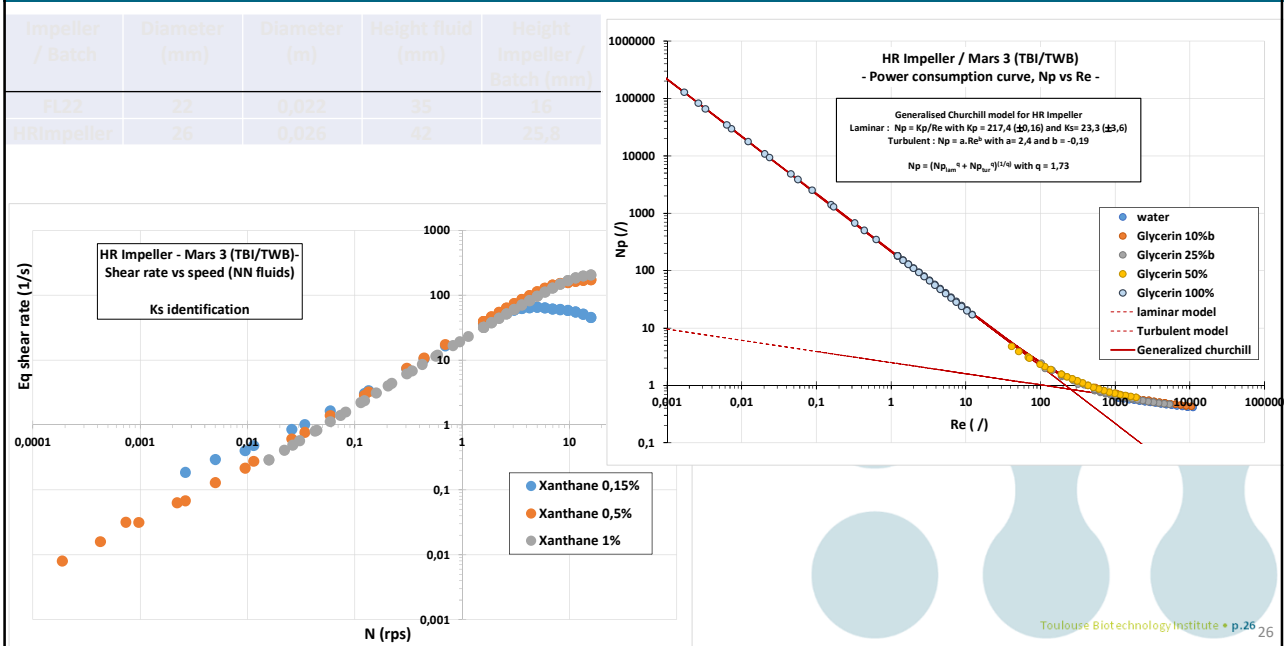


21. RHEOMETRY: EXPERIMENTAL STRATEGY & SOLUTIONS

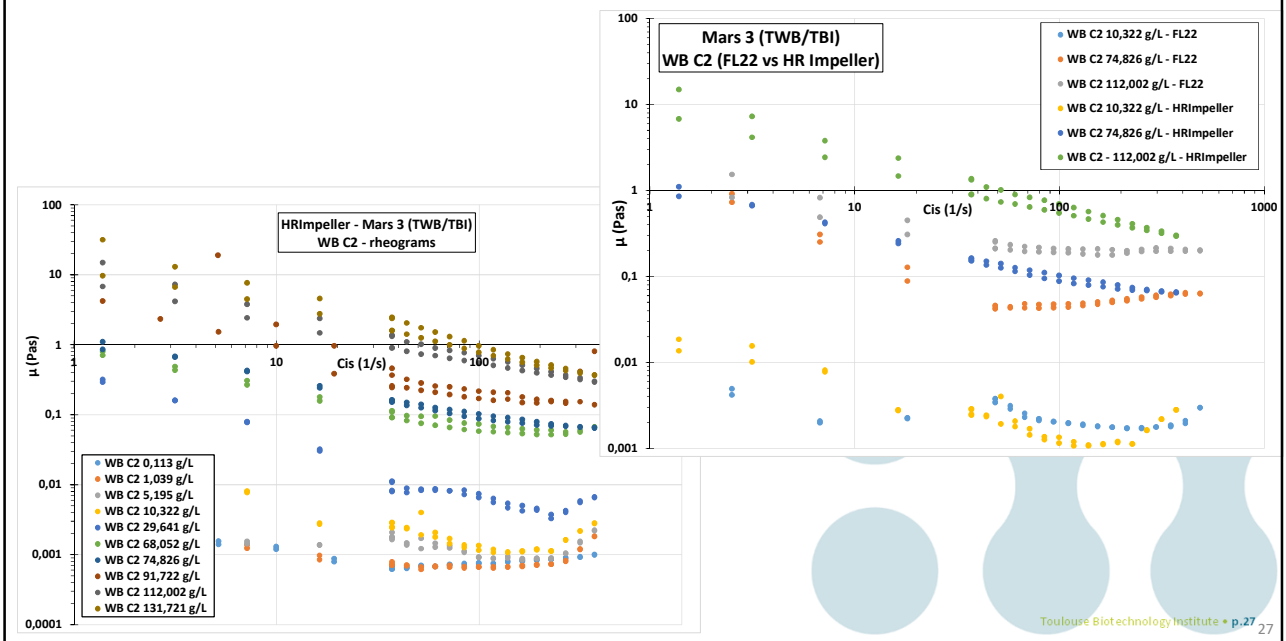
Solution	1st step			2nd step	
	CP60/1°	PP35	CC B27DG	Vanne	Impeller HR
Water	OK	OK	OK	OK	OK
Glycerin 10%	OK	OK	OK	OK	OK
Glycerol 25%	OK	OK	OK	OK	OK
Glycerol 50%	OK	OK	OK	OK	OK
Glycerol 100%	OK	OK	OK	OK	OK
Xanthane 0,15%	OK	OK	OK	OK	OK
Xanthane 0,5%	OK	OK	OK	OK	OK
Xanthane 1%	OK	OK	OK	OK	OK
WB vs cc (0 to 150 gdm/L) and class	/	/	/	OK	OK

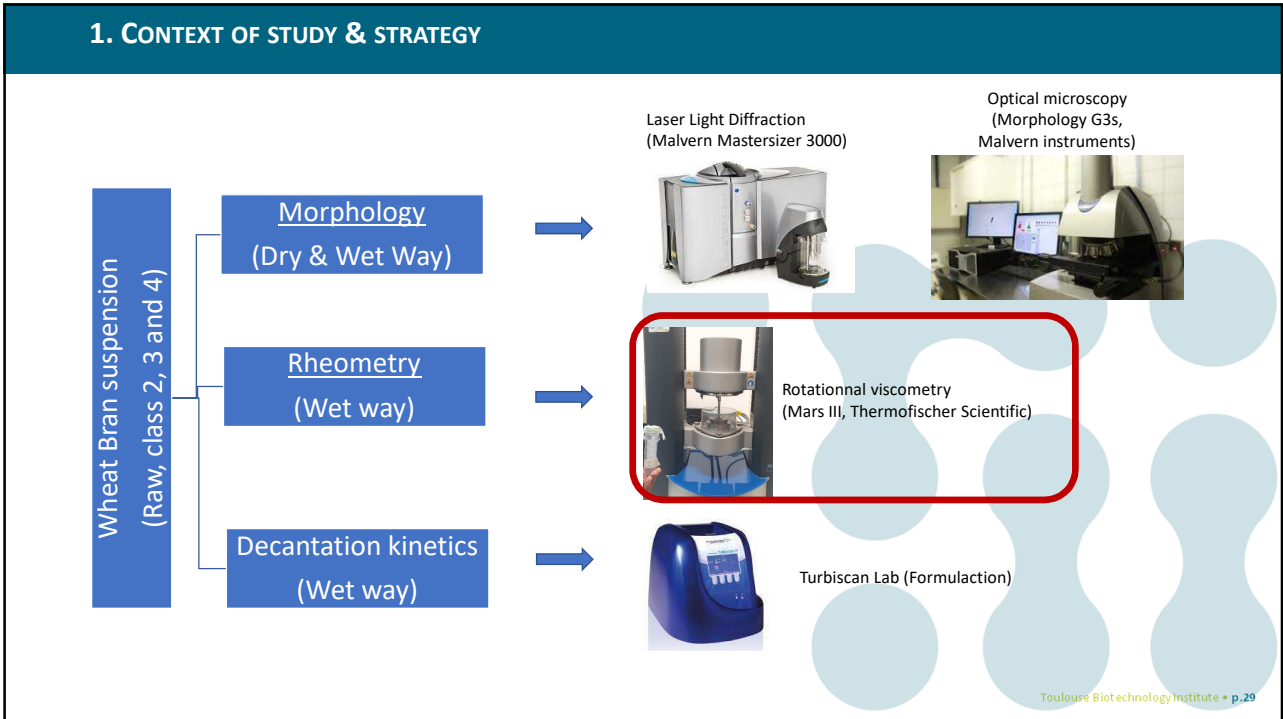


41. RHEOMETRY: POWER CONSUMPTION CURVES (HR IMPELLER)



42. WB RHEOGRAMS (CLASS 2): FL22 & HRIMPELLER





Active ingredients of the formulation

Ingredient	%	Quantity/100g	function
Molasses	5	5.95 g	UV protectant
water		4 mL	
sorbitol	2	2 g	Suspending agent
Corn steep	2	2 g	phagostimulant
Tween 80	0.10	0.1 g = 2 drops	emulsifier
Calcium stearate	2	2 g	lubricant
water		2 mL	
<i>Bt</i> pellet (spores+proteins)	7 or 14	Depends on the desired proteins content and the dry weight of the pellet	Active ingredient
water		48 mL	
Lactose (in the fluid bed dryer)	81.9 or 74.9	81.9 or 74.9g	Carrier and protection of the active ingredient